

12 **EUROPEAN PATENT APPLICATION**

21 Application number: 88311659.2

51 Int. Cl.4: **C07D 307/08 , C07D 307/32 ,**
//B01J23/06,B01J23/72

22 Date of filing: 09.12.88

30 Priority: 23.12.87 US 137042
15.08.88 US 231940

43 Date of publication of application:
28.06.89 Bulletin 89/26

54 Designated Contracting States:
AT BE CH DE ES FR GB GR IT LI LU NL SE

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54 **Vapor-phase hydrogenation of maleic anhydride to tetrahydrofuran and gamma-butyrolactone.**

57 Tetrahydrofuran and optionally gamma-butyrolactone are prepared from at least one of maleic anhydride or succinic anhydride by catalytically hydrogenating vaporous maleic anhydride or vaporous succinic anhydride in the presence of hydrogen and a catalyst comprising the mixed oxides of copper, zinc and aluminum.

EP 0 322 140 A1

VAPOR-PHASE HYDROGENATION OF MALEIC ANHYDRIDE TO TETRAHYDROFURAN AND GAMMA-BUTYROLACTONE

REFERENCE TO RELATED APPLICATIONS

5 This is a continuation-in-part of U.S. application Serial No. 137,042, filed December 23, 1987.

BACKGROUND OF THE INVENTION

Field of the Invention

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15 This invention relates to the preparation of tetrahydrofuran and gamma-butyrolactone from at least one of maleic anhydride or succinic anhydride. In one embodiment this invention relates to a single stage process for the vapor phase hydrogenation of maleic anhydride or succinic anhydride in the presence of a catalyst comprising the mixed oxides of copper, zinc and aluminum to produce high yields of tetrahydrofuran. In another embodiment, this invention relates to a single stage process for the vapor phase hydrogenation of maleic anhydride or succinic anhydride in the presence of a catalyst comprising the mixed
20 oxides of copper, zinc and aluminum to produce high yields of tetrahydrofuran and gamma-butyrolactone.

Description of the Prior Art

25 Tetrahydrofuran is a useful solvent for natural and synthetic resins and is a valuable intermediate in the manufacture of a number of chemicals and plastics. Gamma-butyrolactone is an intermediate for the synthesis of butyric acid compounds, polyvinylpyrrolidone and methionine. Gamma-butyrolactone is a useful solvent for acrylate and styrene polymers and also a useful ingredient of paint removers and textile assistants.

30 It is known in the art that tetrahydrofuran and gamma-butyrolactone may be produced by a number of different methods. For example, tetrahydrofuran is produced by the dehydration of 1,4-butanediol and gamma-butyrolactone can be prepared by the dehydrogenation of 1,4-butanediol. Specifically, most tetrahydrofuran and gamma-butyrolactone is manufactured in a multi-step sequence starting with the reaction of acetylene and formaldehyde in the presence of a cuprous acetylide complex to form butynediol.
35 The butynediol is reduced to butanediol, which is dehydrated to tetrahydrofuran and dehydrogenated to gamma-butyrolactone as indicated above.

In addition, tetrahydrofuran and gamma-butyrolactone can be prepared by catalytic hydrogenation of maleic acid, fumaric acid and succinic acid, their respective anhydrides and ester derivatives.

40 The instant invention focuses on the production of tetrahydrofuran and tetrahydrofuran with gamma-butyrolactone from maleic anhydride. A multi-step process for producing tetrahydrofuran and gamma-butyrolactone in addition to 1,4-butanediol from maleic anhydride is described in U.S. Patent 4,584,419. In this patent the ethyl diester of maleic anhydride is produced and then hydrogenated in the presence of a copper-chromite catalyst to yield minor quantities of tetrahydrofuran and larger quantities of 1,4-butanediol and gamma-butyrolactone.

45 Tetrahydrofuran and gamma-butyrolactone are derived from maleic anhydride or succinic anhydride using nickel base catalysts in U.S. Patent 3,853,922 and U.S. Patent 3,829,448.

Lastly, U.S. Patent 3,894,054 describes a vapor phase process for the conversion of maleic anhydride to tetrahydrofuran using a two component catalyst system consisting of a Cu/Zn/Cr catalyst and a silica-alumina catalyst which has been calcined at approximately 1000° C.

50 An object of this invention is to provide a process for producing tetrahydrofuran and optionally gamma-butyrolactone from maleic anhydride and succinic anhydride in high yields using a single component catalyst and without first esterifying the anhydride. Another object is to provide an efficient catalyst which will produce tetrahydrofuran and optionally gamma-butyrolactone in high yields in a single hydrogenation step with less by-products. Still another object is to provide a novel hydrogenation catalyst which maintains

high activity over time.

SUMMARY OF THE INVENTION

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Maleic anhydride is catalytically hydrogenated to produce tetrahydrofuran or tetrahydrofuran and gamma-butyrolactone in a continuous single stage process. It has been discovered that high yields of tetrahydrofuran or the combination of tetrahydrofuran and gamma-butyrolactone are achieved when the
10 hydrogenation catalyst comprises the mixed oxides of copper, zinc and aluminum.

DETAILED DESCRIPTION OF THE INVENTION

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Maleic anhydride or succinic anhydride are hydrogenated in the vapor phase by passing a mixture of a hydrogen containing gas and the anhydride over a hydrogenation catalyst comprising the mixed oxides of copper, zinc and aluminum.

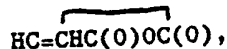
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Reactants

At least one of maleic anhydride or succinic anhydride is fed continuously together with hydrogen, and without further treatment or working-up, over a hydrogenation catalyst.

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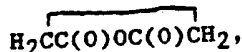
Maleic anhydride,



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is derived from a number of sources. Mostly maleic anhydride is produced by passing a mixture of benzene or butane over a vanadium oxide catalyst at about 450°C. Maleic anhydride is also produced as a by-product from the manufacture of phthalic anhydride from naphthalene or by the catalytic oxidation of butylenes. Succinic anhydride,

35



40 may be produced by the dehydration of succinic acid but is most commonly produced by the direct hydrogenation of maleic anhydride.

Typically, the hydrogen (H₂) containing gas is commercially pure hydrogen. However, the hydrogen containing gas in addition to hydrogen (H₂) may also contain nitrogen (N₂), oxygen (O₂), any gaseous hydrocarbon (e.g. methane), as well as gaseous oxides of carbon, (e.g. carbon monoxide, carbon dioxide).

45

Catalyst

The instant process for the hydrogenation of at least one of maleic anhydride or succinic anhydride to produce tetrahydrofuran is characterized by the use of a hydrogenation catalyst comprising the mixed
50 oxides of copper, zinc and aluminum.

Typically, the hydrogenation catalyst comprising the mixed oxides of copper, zinc and aluminum are of the general formula:



55 where M is at least one element selected from Groups IIA and IIIA, Group VA, Group VIII, Ag, Au Groups IIIB thru VIIB, the Lanthanum Series, and Actinium Series of the Period Table of Elements

$0.001 < b < 500$;

$0.001 < c < 500$;

$0 \leq d < 200$; and

x is the number of oxygen atoms necessary to satisfy the valency requirements of the other elements.

- 5 As used herein, the Periodic Table of Elements refers to the commonly accepted version as appears in The Condensed Chemical Dictionary, 10th Edition, G. G. Hawley, Van-Nostrand Reinhold Company (1981), p. 789. Preferably, the catalyst identified by the above formula contains greater than 10 wt percent of aluminum and more preferably greater than 15 wt percent of aluminum.

10 Copper chromium containing hydrogenation catalysts are known in the art. The catalyst shown by the above formula optionally contains chromium, iron, nickel and cobalt; however, an excellent catalyst of the above formula may be produced with no chromium, no iron, no nickel or no cobalt contained in the catalyst.

Typically, the catalysts of the present invention may be prepared by conventional techniques including coprecipitation techniques such as those described in Preparation of Catalysts III, Hoffstadt et al., Elsevier Science Publishers B.V., (1983) pgs. 709-721. In general, this technique comprises coprecipitation of an aqueous metal nitrate solution at elevated temperatures with an alkali or ammonium carbonate or bicarbonate. The precipitated material is then filtered off, washed and then dried at elevated temperatures (120 °C) and calcined at a temperature of 350-400 °C. The catalyst could also be impregnated with one or more promoter elements prior to the calcination step. Alternatively, promoter elements could be incorporated in the precipitation step.

20 Prior to use, the catalyst may be reduced at temperatures between 150-500 °C by flowing hydrogen, or hydrogen mixed with an inert gas (e.g. nitrogen) over the catalyst. Other reducing gas mixtures may also be used, such as carbon monoxide, carbon monoxide/hydrogen, and carbon monoxide/water. The reduction may be carried out at atmospheric or elevated pressures.

Typically, sufficient catalyst is packed into a fixed-bed or fluid-bed reactor and the reactants passed over and/or through a catalyst bed for continuous operation. In a batch operation, typically 0.1 and about 10 wt%, and preferably between about 1 and about 5 wt% of catalyst is used based upon the weight of the maleic anhydride or succinic anhydride to be converted.

30 Process Parameters

At least one of maleic anhydride or succinic anhydride (in the absence of added water) are co-fed with a hydrogen-containing gas over the hydrogenation catalyst, at elevated temperature and pressures. The hydrogen to anhydride molar feed ratio may vary from about 10:1 to about 1000:1, and is preferably between about 50:1 and 500:1.

35 The hydrogen containing gas can be introduced into the hydrogenation apparatus together with the maleic anhydride or succinic anhydride mixture, co-currently or counter-currently. Typically, the anhydride is vaporized in a hot hydrogen containing gas stream and this mixture is then passed over the hydrogenation catalyst. In order to enhance process economics, unreacted hydrogen discharged from the hydrogenation reaction may be recycled to the hydrogenation furnace.

40 The quality of the results of the hydrogenation reaction is partially dependent on the throughput of the anhydride-hydrogen mixture over the catalyst. The throughput for the successful performance of the reaction can vary within wide limits. For example, the maleic anhydride or succinic anhydride liquid hourly space velocity (LHSV) is between about 0.01 and 10 per hour, the hydrogen containing gas hourly space velocity (GHSV) is between about 100 to 500,000 per hour. The LHSV and GHSV rates used herein are the feed rates of the reactants prior to vaporization of the anhydride. At these rates the contact time is considerably less than one hour. Preferably contact times are less than 1 minute and more preferably less than 20 seconds. Typical reaction times are between 2 and 10 seconds.

45 The vaporous feed mixture is contacted with the hydrogenation catalyst at pressures of 1 to 500 atmospheres, preferably at 1 to 100 atmospheres, more preferably at about 1 to 50 atmospheres hydrogen pressure. Suitable reaction temperatures are 200 °C to 400 °C and are preferably 220 °C to 300 °C.

Hydrogenation furnaces of conventional construction can be used for carrying out the process of this invention, provided that they are designed for the requisite temperatures and pressures and are made of acid-resistant material. Further, the process may be carried out in a variety of reactors including fixed-bed and fluid-bed systems.

55 The reaction products (predominantly tetrahydrofuran or tetrahydrofuran and gamma-butyrolactone) are advantageously separated by fractional distillation. By-products which are formed in small amounts or unreacted feed, such as, for example, succinic anhydride are advantageously returned to the hydrogenation

stage. Small proportions of acidic by-products in the product can be removed by treatment with alkali before distillation.

Using the process of this invention, maleic anhydride or succinic anhydride is converted virtually quantitatively (i.e., 100 percent conversion of feed to products and by-products) in a simple reaction, without the build-up of coke or tar inside the reactor. The yields of tetrahydrofuran achieved are greater than 90 mole percent, e.g., 91-98 mole percent. The formation of non-utilizable by-products is slight. Tetrahydrofuran which is more than 99.5 percent pure can be recovered and separated from the reaction products by fractional distillation.

Gamma-butyrolactone is an intermediate in the hydrogenation of maleic anhydride or succinic anhydride to tetrahydrofuran. It has been theorized that the existence of succinic anhydride in the reactor strongly inhibits the adsorption of the gamma-butyrolactone onto the catalyst. This means that less tetrahydrofuran is formed when succinic anhydride is concentrated at the catalyst; but as the amount of succinic anhydride decreases, the rapid formation of tetrahydrofuran begins. Consequently, if the reaction is stopped just before the rapid transformation of gamma-butyrolactone to tetrahydrofuran or if the rate at which gamma-butyrolactone is transformed to tetrahydrofuran is slowed, then more gamma-butyrolactone will appear in the product. Methods for accomplishing this and controlling the proportions of tetrahydrofuran and gamma-butyrolactone produced include adjusting the process parameters of (i) temperature, and/or (ii) pressure, and/or (iii) maleic anhydride and succinic anhydride throughput, and/or (iv) maleic anhydride and succinic anhydride partial pressure. For example, (i) increasing the temperature, while maintaining other reaction parameters constant, will favor the production of tetrahydrofuran; (ii) increasing the throughput, while maintaining other reaction parameters constant, will favor gamma-butyrolactone production; and (iii) increasing the partial pressure of the anhydride, while maintaining the overall anhydride throughput and the other reaction parameters constant, will favor gamma-butyrolactone production. Consequently, gamma-butyrolactone in addition to tetrahydrofuran may be produced by the instant invention in recoverable quantities approaching a 1:4 ratio of tetrahydrofuran to gamma-butyrolactone and combined yields of 90 moles percent or greater.

Although the preceding description is given in terms of a continuous process, if desired, the process of this invention may be carried out in batch mode employing conditions corresponding to those specified above. Without further elaboration, it is believed that one skilled in the art can, using the preceding description, utilize the present invention to its fullest extent.

SPECIFIC EMBODIMENT

The following preferred embodiments are to be construed as merely illustrative, and not limitative of the remainder of the disclosure in any way whatsoever. The percent yields in all examples result from 100 percent conversion of the feed to the products and by-products.

Example 1

A commercially available catalyst comprising the mixed oxides of copper, zinc, aluminum and chromium is employed in Example 1. The oxidized form of this catalyst is of the general formula $\text{CuO/ZnO/Al}_2\text{O}_3/\text{Cr}_2\text{O}_3$. The nominal compositions of the unreduced catalyst is as follows:

Copper Oxide	40-50 wt%
Zinc Oxide	10-20 wt%
Alumina	20-30 wt%
Chrome Oxide	1-5 wt%

This catalyst has an empirical formula of $\text{Cu}_{1.0}\text{Al}_{1.2}\text{Zn}_{0.4}\text{Cr}_{0.04}\text{O}_x$.

The catalyst was obtained in 1/8" pellet form. The pellets were ground and sieved to obtain 10/30 mesh fractions which were used for catalyst testing.

20 cc of the $\text{CuO/ZnO/Al}_2\text{O}_3/\text{Cr}_2\text{O}_3$ catalyst (21.4g) was loaded into a 40 cc tubular stainless steel reactor. The catalyst was reduced at 250° C and atmospheric pressure, with a gas mixture of 5% H_2 in N_2 .

flowing over the catalyst at a rate of 1 standard liters per minute (SLM).

After reduction, the system was pressurized to 600 psig and a mixture of vaporized maleic anhydride in hydrogen was passed over the catalyst. The H₂/MAH mixture was prepared by pumping molten maleic anhydride in a stream of hydrogen in a vaporizer at 155 °C. The details and results of the catalyst testing between 235 °C and 250 °C are summarized in Table I below:

TABLE I

Hydrogenation of MAH over CuO/ZnO/Al ₂ O ₃ /Cr ₂ O ₃				
Temperature (°C)	235	240	250	250
MAH Partial Pressure (atm)	0.139	0.131	0.127	0.208
Contact Time (sec)	13.5	8.4	5.9	6.1
H ₂ GHSV (h ⁻¹)	5840	9320	12520	12505
MAH LHSV (h ⁻¹)	0.068	0.101	0.135	0.216
Percent Yield				
THF	92	98	95	96
Butane	0.7	0.8	2.3	1.2
Butanol	2.5	2.0	2.8	2.2
Propanol	0.2	0.16	0.22	0.26
Methanol	0.05	0.04	0.05	0.04
Pressure = 600 psig				

Table I illustrates that the process of the instant invention produces high yields of tetrahydrofuran over a range of throughputs and maleic anhydride to hydrogen ratios.

Example 2

The CuO/ZnO/Al₂O₃/Cr₂O₃ hydrogenation catalyst, as used in Example 1, was obtained in 1/8" pellet form. The pellets were calcined at 450 °C and then ground and meshed to obtain a 20/30 mesh fraction. 5 cc of this catalyst was diluted with 15 cc of quartz chips of the same mesh size and then loaded into a 40 cc tubular stainless steel reactor. The catalyst was reduced at 250-270 °C in a 5% H₂/N₂ gas mixture flowing at 1 SLM.

Catalyst testing was carried out at 300 psig and 250-270 °C. Maleic anhydride was vaporized into a hydrogen stream at 155 °C. This mixture was then transferred via a heated line to the reactor. The test results are summarized in Table II below:

TABLE II

Hydrogenation of MAH over CuO/ZnO/Al ₂ O ₃ /Cr ₂ O ₃ in Quartz Catalyst									
TOS h	Temperature °C	LHSV h ⁻¹	GHSV h ⁻¹	% YIELDS					
				THF	GBL	SAH	BDO	ROH	GAS
51	270	0.81	66100	64.1	23.7	2.5	0.6	2.5	0.41
194	250	0.27	22025	36.3	52.4	8.6	0.3	1.2	0.25
290	250	0.27	22025	31.4	50.6	10.3	0.2	1.2	0.25
314	250	0.27	22025	31.9	51.3	10.4	0.3	1.2	0.25
TOS = Time on Stream THF = Tetrahydrofuran GBL = Gamma-Butyrolactone SAH = Succinic Anhydride BDO = 1,4-Butanediol ROH = Propanol and Butanol GAS = CH ₄ , CO ₂ and Butane									

Table II illustrates that high yields of both tetrahydrofuran and gamma-butyrolactone are achievable in the instant process. Also, the above data illustrates that less tetrahydrofuran and more gamma-butyrolactone can be produced in the instant process by adjusting the process parameters.

Example 3

The CuO/ZnO/Al₂O₃/Cr₂O₃ hydrogenation catalyst, as used in Example 1, was obtained in 1/8" pellet form. The pellets were calcined at 450° C and then ground and meshed to obtain a 20/30 mesh fraction. 5 cc of this catalyst was diluted with 15 cc of a low surface area alumina (Harshaw Al-390T). The alumina, obtained as 1/8" pellets was ground and meshed to give a 20/30 mesh fraction. The catalyst and alumina were loaded into a 40 cc tubular stainless steel reactor. The catalyst was then reduced and tested as described in Example 2. The test results are summarized in Table III below.

TABLE III

Hydrogenation of MAH over CuO/ZnO/Al ₂ O ₃ /Cr ₂ O ₃ in Alumina Catalyst									
TOS h	Temperature °C	LHSV h ⁻¹	GHSV h ⁻¹	% YIELDS					
				THF	GBL	SAH	BDO	ROH	GAS
349	265	0.66	50400	83.6	11.5	1.1	0	2.6	1.1
564	270	0.66	50400	93.7	1.3	0	0	3.7	1.4

Table III illustrates that greater yields of tetrahydrofuran are achieved by increasing the process temperature while maintaining the remaining process parameters constant.

Although the invention has been described in considerable detail through the preceding examples, these examples are for the purpose of illustration only and one skilled in the art will understand that variations and modifications can be made without departing from the spirit and scope of the invention.

Claims

1. A continuous process for the preparation of tetrahydrofuran comprising catalytically hydrogenating a vaporous mixture of at least one of maleic anhydride or succinic anhydride in a hydrogen containing gas in contact with a hydrogenation catalyst of the formula:
 $Cu_x Zn_b Al_c M_d O_x$ wherein M is at least one element selected from the group consisting of Groups IIA and IIIA, Group VA, Group VIII, Ag, Au, Groups IIIB thru VIIB, the Lanthanum Series, and Actinium Series.
 $0.001 < b < 500$;
 $0.001 < c < 500$;
 $0 \leq d < 200$; and
x is the number of oxygen atoms necessary to satisfy the valency requirements of the other elements.
2. The process of claim 1, wherein tetrahydrofuran and gamma-butyrolactone are produced.
3. The process of claim 1, wherein the reaction time is less than 1 minute.
4. The process of claim 3, wherein the hydrogenation catalyst contains greater than 10 weight percent aluminum.
5. The process of claim 4, wherein the hydrogenation catalyst contains greater than 15 weight percent aluminum.
6. The process of claim 1, wherein the hydrogen to anhydride feed ratio is between about 10 to 1 and 1000 to 1.
7. The process of claim 6, wherein the hydrogen to the anhydride feed ratio is between about 50 to 1 and 500 to 1.
8. The process of claim 1, wherein the hydrogenation is conducted at a pressure about 1 to 100 atmospheres and at a temperature of about 200° C to 400° C.
9. The process of claim 8, wherein the hydrogenation is conducted at a pressure of about 1 to 50 atmospheres and at a temperature of about 220° C to 300° C.
10. The process of claim 1, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminum in the absence of chromium.
11. The process of claim 1, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminum in the absence of iron.
12. The process of claim 1, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminum in the absence of nickel.
13. The process of claim 1, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminum in the absence of cobalt.



European Patent
Office

EUROPEAN SEARCH REPORT

Application Number

EP 88 31 1659

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)
A	DE-A-2,332,906 (KAO SOAP CO) * page 9, claim 1 * & US - A - 38 94054 (Cat. D) ---	1	C 07 D 307/08 C 07 D 307/32 // B 01 J 23/06 B 01 J 23/72
A	US-A-4 001 282 (ELWOOD M. MILLER) * column 3, example 1; column 5, example 6 * ---	1	
A	FR-A-2 027 162 (CATALYSTS AND CHEMICALS) * page 4, examples 1,2; page 6, table I * ---	1	
A	US-A-4 105 674 (WALDO DE THOMAS et al.) * column 9, claim 1 * -----	1	
			TECHNICAL FIELDS SEARCHED (Int. Cl.4)
			B 01 J 23/00 C 07 D 307/00 C 07 D 315/00
The present search report has been drawn up for all claims			
Place of search BERLIN		Date of completion of the search 17-02-1989	Examiner KYRIAKAKOU G
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons ----- & : member of the same patent family, corresponding document			



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European Patent Office
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(11) Publication number: **0 322 140 B1**

(12)

EUROPEAN PATENT SPECIFICATION

- (45) Date of publication of patent specification: **19.11.92** (51) Int. Cl.⁵: **C07D 307/08, C07D 307/32, //B01J23/06, B01J23/72**
- (21) Application number: **88311659.2**
- (22) Date of filing: **09.12.88**

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- (30) Priority: **23.12.87 US 137042**
15.08.88 US 231940
- (43) Date of publication of application:
28.06.89 Bulletin 89/26
- (45) Publication of the grant of the patent:
19.11.92 Bulletin 92/47
- (84) Designated Contracting States:
AT BE CH DE ES FR GB GR IT LI LU NL SE
- (56) References cited:
DE-A- 2 332 906
FR-A- 2 027 162
US-A- 4 001 282
US-A- 4 105 674

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Description

This invention relates to the preparation of tetrahydrofuran and gamma-butyrolactone from at least one of maleic anhydride or succinic anhydride. In one embodiment this invention relates to a single stage process for the vapor phase hydrogenation of maleic anhydride or succinic anhydride in the presence of a catalyst comprising the mixed oxides of copper, zinc and aluminum to produce high yields of tetrahydrofuran. In another embodiment, this invention relates to a single stage process for the vapor phase hydrogenation of maleic anhydride or succinic anhydride in the presence of a catalyst comprising the mixed oxides of copper, zinc and aluminum to produce high yields of tetrahydrofuran and gamma-butyrolactone.

Tetrahydrofuran is a useful solvent for natural and synthetic resins and is a valuable intermediate in the manufacture of a number of chemicals and plastics. Gamma-butyrolactone is an intermediate for the synthesis of butyric acid compounds, polyvinylpyrrolidone and methionine. Gamma-butyrolactone is a useful solvent for acrylate and styrene polymers and also a useful ingredient of paint removers and textile assistants.

It is known in the art that tetrahydrofuran and gamma-butyrolactone may be produced by a number of different methods. For example, tetrahydrofuran is produced by the dehydration of 1,4-butanediol and gamma-butyrolactone can be prepared by the dehydrogenation of 1,4-butanediol. Specifically, most tetrahydrofuran and gamma-butyrolactone is manufactured in a multi-step sequence starting with the reaction of acetylene and formaldehyde in the presence of a cuprous acetylide complex to form butynediol. The butynediol is reduced to butanediol, which is dehydrated to tetrahydrofuran and dehydrogenated to gamma-butyrolactone as indicated above.

In addition, tetrahydrofuran and gamma-butyrolactone can be prepared by catalytic hydrogenation of maleic acid, fumaric acid and succinic acid, their respective anhydrides and ester derivatives.

The instant invention focuses on the production of tetrahydrofuran and gamma-butyrolactone from maleic anhydride. A multi-step process for producing tetrahydrofuran and gamma-butyrolactone in addition to 1,4-butanediol from maleic anhydride is described in US Patent 4,584,419. In this patent the ethyl diester of maleic anhydride is produced and then hydrogenated in the presence of a copper-chromite catalyst to yield minor quantities of tetrahydrofuran and larger quantities of 1,4-butanediol and gamma-butyrolactone.

Tetrahydrofuran and gamma-butyrolactone are derived from maleic anhydride or succinic anhydride using nickel base catalysts in US Patent 3,853,922 and US Patent 3,829,448. DE-A-2455617 discloses a multi-step process for the preparation of 1,4-butanediol and/or tetrahydrofuran from maleic anhydride or succinic anhydride.

Lastly, US Patent 3,894,054 describes a vapor phase process for the conversion of maleic anhydride to tetrahydrofuran using a two component catalyst system consisting of a Cu/Zn/Cr catalyst and a silica-alumina catalyst which had been calcined at approximately 1000 °C.

An object of this invention is to provide a process for producing tetrahydrofuran and optionally gamma-butyrolactone from maleic anhydride and succinic anhydride in high yields using a single component catalyst and without first esterifying the anhydride. Another object is to provide an efficient catalyst which will produce tetrahydrofuran and optionally gamma-butyrolactone in high yields in a single hydrogenation step with less by-products. Still another object is to provide a novel hydrogenation catalyst which maintains high activity over time.

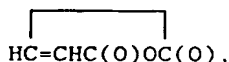
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Maleic anhydride or succinic anhydride are hydrogenated in the vapor phase by passing a mixture of a hydrogen containing gas and the anhydride over a hydrogenation catalyst comprising the mixed oxides of copper, zinc and aluminium.

Reactants

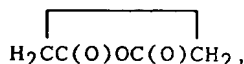
At least one of maleic anhydride or succinic anhydride is fed continuously together with hydrogen, and without further treatment or working-up, over a hydrogenation catalyst.

Maleic anhydride,



5 is derived from a number of sources. Mostly maleic anhydride is produced by passing a mixture of benzene or butane over a vanadium oxide catalyst at about 450 °C. Maleic anhydride is also produced as a by-product from the manufacture of phthalic anhydride from naphthalene or by the catalytic oxidation of butylenes.
Succinic anhydride,

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15 may be produced by the dehydrogenation of succinic acid but is most commonly produced by the direct hydrogenation of maleic anhydride.

Typically, the hydrogen (H₂) containing gas is commercially pure hydrogen. However, the hydrogen containing gas in addition to hydrogen (H₂) may also contain nitrogen (N₂), oxygen (O₂), any gaseous hydrocarbon (e.g. methane), as well as gaseous oxides of carbon, (e.g. carbon monoxide, carbon dioxide).

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Catalyst

The instant process for the hydrogenation of at least one of maleic anhydride or succinic anhydride to produce tetrahydrofuran is characterised by the use of a hydrogenation catalyst comprising the mixed oxides of copper, zinc and aluminium.

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The hydrogenation catalyst comprising the mixed oxides of copper, zinc and aluminium are of the general formula:



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where M is at least one element selected from Groups IIA and IIIA, Group VA, Group VIII, Ag, Au, Groups IIIB thru VIIB, the Lanthanum Series, and Actinium Series of the Period Table of Elements

0.001 < b < 500;

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0.001 < c < 500;

0 ≤ d ≤ 200; and

x is the number of oxygen atoms necessary to satisfy the valency requirements of the other elements.

As used herein, the Periodic Table of Elements refers to the commonly accepted version as appears in The Condensed Chemical Dictionary, 10th Edition, G. G. Hawley, Van-Nostrand Reinhold Company (1981), p. 789. Preferably, the catalyst identified by the above formula contains greater than 10 wt percent of aluminum and more preferably greater than 15 wt percent of aluminum.

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Copper chromium containing hydrogenation catalysts are known in the art. The catalyst shown by the above formula optionally contains chromium, iron, nickel and cobalt; however, an excellent catalyst of the above formula may be produced with no chromium, no iron, no nickel or no cobalt contained in the catalyst.

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Typically, the catalysts of the present invention may be prepared by conventional techniques including coprecipitation techniques such as those described in Preparation of Catalysts III, Hoffstadt et al., Elsevier Science Publishers B.V., (1983) pgs. 709-721. In general, this technique comprises coprecipitation of an aqueous metal nitrate solution at elevated temperatures with an alkali or ammonium carbonate or bicarbonate. The precipitated material is then filtered off, washed and then dried at elevated temperatures (120 °C) and calcined at a temperature of 350-400 °C. The catalyst could also be impregnated with one or more promoter elements prior to the calcination step. Alternatively, promoter elements could be incorporated in the precipitation step.

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Prior to use, the catalyst may be reduced at temperatures between 150-500 °C by flowing hydrogen, or hydrogen mixed with an inert gas (e.g. nitrogen) over the catalyst. Other reducing gas mixtures may also be used, such as carbon monoxide, carbon monoxide/hydrogen, and carbon monoxide/water. The reduction may be carried out at atmospheric or elevated pressures.

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Typically, sufficient catalyst is packed into a fixed-bed or fluid-bed reactor and the reactants passed over and/or through a catalyst bed for continuous operation. In a batch operation, typically 0.1 and about 10

wt%, and preferably between about 1 and about 5 wt% of catalyst is used based upon the weight of the maleic anhydride or succinic anhydride to be converted.

Process Parameters

At least one of maleic anhydride or succinic anhydride (in the absence of added water) are co-fed with a hydrogen-containing gas over the hydrogenation catalyst, at elevated temperature and pressures. The hydrogen to anhydride molar feed ratio may vary from about 10:1 to about 1000:1, and is preferably between about 50:1 and 500:1.

The hydrogen containing gas can be introduced into the hydrogenation apparatus together with the maleic anhydride or succinic anhydride mixture, co-currently or counter-currently. Typically, the anhydride is vaporized in a hot hydrogen containing gas stream and this mixture is then passed over the hydrogenation catalyst. In order to enhance process economics, unreacted hydrogen discharged from the hydrogenation reaction may be recycled to the hydrogenation furnace.

The quality of the results of the hydrogenation reaction is partially dependent on the throughput of the anhydride-hydrogen mixture over the catalyst. The throughput for the successful performance of the reaction can vary within wide limits. For example, the maleic anhydride or succinic anhydride liquid hourly space velocity (LHSV) is between about 0.01 and 10 per hour, the hydrogen containing gas hourly space velocity (GHSV) is between about 100 to 500,000 per hour. The LHSV and GHSV rates used herein are the feed rates of the reactants prior to vaporization of the anhydride. At these rates the contact time is considerably less than one hour. Preferably contact times are less than 1 minute and more preferably less than 20 seconds. Typical reaction times are between 2 and 10 seconds.

The vaporous feed mixture is contacted with the hydrogenation catalyst at pressures of 1.0332 to 516.6 kg/cm² (1 to 500 atmospheres), preferably 1.0332 to 103.32 kg/cm² (1 to 100 atmospheres), more preferably at about 1.0332 to 51.66 kg/cm² (1 to 50 atmospheres) hydrogen pressure. Suitable reaction temperatures are 200°C to 400°C and are preferably 220°C to 300°C.

Hydrogenation furnaces of conventional construction can be used for carrying out the process of this invention, provided that they are designed for the requisite temperatures and pressures and are made of acid-resistant material. Further, the process may be carried out in a variety of reactors including fixed-bed and fluid-bed systems.

The reaction products (predominantly tetrahydrofuran or tetrahydrofuran and gamma-butyrolactone) are advantageously separated by fractional distillation. By-products which are formed in small amounts or unreacted feed, such as, for example, succinic anhydride are advantageously returned to the hydrogenation stage. Small proportions of acidic by-products in the product can be removed by treatment with alkali before distillation.

Using the process of this invention, maleic anhydride or succinic anhydride is converted virtually quantitatively (i.e., 100 percent conversion of feed to products and by-products) in a simple reaction, without the build-up of coke or tar inside the reactor. The yields of tetrahydrofuran achieved are greater than 90 mole percent, e.g. 91-98 mole percent. The formation of non-utilizable by-products is slight. Tetrahydrofuran which is more than 99.5 percent pure can be recovered and separated from the reaction products by fractional distillation.

Gamma-butyrolactone is an intermediate in the hydrogenation of maleic anhydride or succinic anhydride to tetrahydrofuran. It has been theorized that the existence of succinic anhydride in the reactor strongly inhibits the adsorption of the gamma-butyrolactone onto the catalyst. This means that less tetrahydrofuran is formed when succinic anhydride is concentrated at the catalyst; but as the amount of succinic anhydride decreases, the rapid formation of tetrahydrofuran begins. Consequently, if the reaction is stopped just before the rapid transformation of gamma-butyrolactone to tetrahydrofuran or if the rate at which gamma-butyrolactone is transformed to tetrahydrofuran is slowed, then more gamma-butyrolactone will appear in the product. Methods for accomplishing this and controlling the proportions of tetrahydrofuran and gamma-butyrolactone produced include adjusting the process parameters of (i) temperature, and/or (ii) pressure, and/or (iii) maleic anhydride and succinic anhydride throughput, and/or (iv) maleic anhydride and succinic anhydride partial pressure. For example, (i) increasing the temperature, while maintaining other reaction parameters constant, will favor the production of tetrahydrofuran; (ii) increasing the throughput, while maintaining other reaction parameters constant, will favor gamma-butyrolactone production; and (iii) increasing the partial pressure of the anhydride, while maintaining the overall anhydride throughput and the other reaction parameters constant, will favor gamma-butyrolactone production. Consequently, gamma-butyrolactone in addition to tetrahydrofuran may be produced by the instant invention in recoverable quantities approaching a 1:4 ratio of tetrahydrofuran to gamma-butyrolactone and combined yields of 90

moles percent or greater.

Although the preceding description is given in terms of a continuous process, if desired, the process of this invention may be carried out in batch mode employing conditions corresponding to those specified above. Without further elaboration, it is believed that one skilled in the art can, using the preceding description, utilize the present invention to its fullest extent.

The invention will now be illustrated by the following Examples. The percent yields in all examples result from 100 percent conversion of the feed to the products and by-products.

Example 1

A commercially available catalyst comprising the mixed oxides of copper, zinc, aluminium and chromium is employed in Example 1. The oxidized form of this catalyst is of the general formula $\text{CuO/ZnO/Al}_2\text{O}_3\text{/Cr}_2\text{O}_3$. The nominal compositions of the unreduced catalyst is as follows:

Copper Oxide	40-50 wt%
Zinc Oxide	10-20 wt%
Alumina	20-30 wt%
Chrome Oxide	1-5 wt%

This catalyst has an empirical formula of $\text{Cu}_{1.0}\text{Al}_{1.2}\text{Zn}_{0.4}\text{Cr}_{0.04}\text{O}_x$.

The catalyst was obtained in a 1/8" pellet form. The pellets were ground and sieved to obtain 10/30 mesh fractions which were used for catalyst testing.

20 cc of the $\text{CuO/ZnO/Al}_2\text{O}_3\text{/Cr}_2\text{O}_3$ catalyst (21.4 g) was loaded into a 40 cc tubular stainless steel reactor. The catalyst was reduced at 250 °C and atmospheric pressure, with a gas mixture of 5% H_2 in N_2 flowing over the catalyst at a rate of 1 standard litres per minute (SLM).

After reduction, the system was pressurised to 42.18 kg/cm² (600 psig) and a mixture of vaporised maleic anhydride in hydrogen was passed over the catalyst. The H_2 /MAH mixture was prepared by pumping molten maleic anhydride in a stream of hydrogen in a vaporiser at 155 °C. The details and results of the catalyst testing between 235 °C and 250 °C are summarised in Table I below:

TABLE I

Hydrogenation of MAH over $\text{CuO/ZnO/Al}_2\text{O}_3\text{/Cr}_2\text{O}_3$				
Temperature (°C)	235	240	250	250
MAH Partial Pressure kg/cm ² (atm)	0.144 (0.139)	0.135 (0.131)	0.131 (0.127)	0.215 (0.208)
Contact Time (sec)	13.5	8.4	5.9	6.1
H_2 GHSV (h^{-1})	5840	9320	12520	12505
MAH LHSV (h^{-1})	0.068	0.101	0.135	0.216
Percent Yield				
THF	92	98	95	96
Butane	0.7	0.8	2.3	1.2
Butanol	2.5	2.0	2.8	2.2
Propanol	0.2	0.16	0.22	0.26
Methanol	0.05	0.04	0.05	0.04
Pressure = 42.18 kg/cm ² (600 psig)				

Table I illustrates that the process of the instant invention produces high yields of tetrahydrofuran over a range of throughputs and maleic anhydride to hydrogen ratios.

Example 2

The $\text{CuO/ZnO/Al}_2\text{O}_3\text{/Cr}_2\text{O}_3$ hydrogenation catalyst, as used in Example 1, was obtained in 1/8" pellet form. The pellets were calcined at 450 °C and then ground and meshed to obtain a 20/30 mesh fraction. 5 cc of this catalyst was diluted with 15 cc of quartz chips of the same mesh size and then loaded into a 40

cc tubular stainless steel reactor. The catalyst was reduced at 250-270 °C in a 5% H₂/N₂ gas mixture flowing at 1 SLM.

Catalyst testing was carried out at 21.09 kg/cm² (300 psig) and 250-270 °C. Maleic anhydride was vaporised into a hydrogen stream at 155 °C. This mixture was then transferred via a heated line to the reactor. The test results are summarised in Table II below:

TABLE II

Hydrogenation of MAH over CuO/ZnO/Al ₂ O ₃ /Cr ₂ O ₃ in Quartz Catalyst									
TOS h	Temperature °C	LHSV h ⁻¹	GHSV h ⁻¹	% YIELDS					
				THF	GBL	SAH	BDO	ROH	GAS
51	270	0.81	66100	64.1	23.7	2.5	0.6	2.5	0.41
194	250	0.27	22025	36.3	52.4	8.6	0.3	1.2	0.25
290	250	0.27	22025	31.4	50.6	10.3	0.2	1.2	0.25
314	250	0.27	22025	31.9	51.3	10.4	0.3	1.2	0.25
TOS = Time on Stream THF = Tetrahydrofuran GBL = Gamma-Butyrolactone SAH = Succinic Anhydride BDO = 1,4-Butanediol ROH = Propanol and Butanol GAS = CH ₄ , CO ₂ and Butane									

Table II illustrates that high yields of both tetrahydrofuran and gamma-butyrolactone are achievable in the instant process. Also, the above data illustrates that less tetrahydrofuran and more gamma-butyrolactone can be produced in the instant process by adjusting the process parameters.

Example 3

The CuO/ZnO/Al₂O₃/Cr₂O₃ hydrogenation catalyst, as used in Example 1, was obtained in 1/8" pellet form. The pellets were calcined at 450 °C and then ground and meshed to obtain a 20/30 mesh fraction. 5 cc of this catalyst was diluted with 15 cc of a low surface area alumina (Harshaw Al-390T). The alumina, obtained as 1/8" pellets was ground and meshed to give a 20/30 mesh fraction. The catalyst and alumina were loaded into a 40 cc tubular stainless steel reactor. The catalyst was then reduced and tested as described in Example 2. The test results are summarized in Table III below.

TABLE III

Hydrogenation of MAH over CuO/ZnO/Al ₂ O ₃ /Cr ₂ O ₃ in Alumina Catalyst									
TOS h	Temperature °C	LHSV h ⁻¹	GHSV h ⁻¹	% Yields					
				THF	GBL	SAH	BDO	ROH	GAS
349	265	0.66	50400	83.6	11.5	1.1	0	2.6	1.1
564	270	0.66	50400	93.7	1.3	0	0	3.7	1.4

Table III illustrates that greater yields of tetrahydrofuran are achieved by increasing the process temperature while maintaining the remaining process parameters constant.

Claims

1. A continuous single stage process for the preparation of tetrahydrofuran or tetrahydrofuran and gamma-butyrolactone comprising catalytically hydrogenating a vaporous mixture of at least one of maleic anhydride or succinic anhydride in a hydrogen containing gas in contact with a single hydrogenation

catalyst of the formula:



- 5 wherein M is at least one element selected from the group consisting of Groups IIA and IIIA, Group VA, Group VIII, Ag, Au, Groups IIIB thru VIIB, the Lanthanum Series, and Actinium Series,
 $0.001 < b < 500$;
 $0.001 < c < 500$;
 10 $0 \leq d < 200$; and
 x is the number of oxygen atoms necessary to satisfy the valency requirements of the other elements.

2. The process of claim 1, wherein tetrahydrofuran and gamma-butyrolactone are produced.
- 15 3. The process of claim 1, wherein the reaction time is less than 1 minute.
4. The process of claim 3, wherein the hydrogenation catalyst contains greater than 10 weight percent aluminium.
- 20 5. The process of claim 4, wherein the hydrogenation catalyst contains greater than 15 weight percent aluminium.
6. The process of claim 1, wherein the hydrogen to anhydride feed ratio is between 10 to 1 and 1000 to 1.
- 25 7. The process of claim 6, wherein the hydrogen to the anhydride feed ratio is between 50 to 1 and 500 to 1.
8. The process of claim 1, wherein the hydrogenation is conducted at a pressure 1.0332 to 103.32 kg/cm² (1 to 100 atmospheres) and at a temperature of 220 °C to 400 °C.
- 30 9. The process of claim 8, wherein the hydrogenation is conducted at a pressure of 1.0332 to 51.66 kg/cm² (1 to 50 atmospheres) and at a temperature of 220 °C to 300 °C.
10. The process of any of claims 1 to 9 wherein the catalyst comprises the mixed oxides of copper, zinc, aluminium and optionally contains chromium, iron, nickel and cobalt.
- 35 11. The process of claim 10, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminium in the absence of chromium.
- 40 12. The process of claim 10, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminium in the absence of iron.
13. The process of claim 10, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminium in the absence of nickel.
- 45 14. The process of claim 10, wherein the catalyst comprises the mixed oxides of copper, zinc and aluminium in the absence of cobalt.

Patentansprüche

- 50 1. Kontinuierliches, einstufiges Verfahren zur Herstellung von Tetrahydrofuran oder Tetrahydrofuran und gamma-Butyrolacton, umfassend ein katalytisches Hydrieren eines dampfförmigen Gemisches wenigstens eines Vertreters von Maleinsäureanhydrid oder Bernsteinsäureanhydrid in einem Wasserstoff enthaltenden Gas in Kontakt mit einem einzigen Hydrierkatalysator mit der Formel:



worin M wenigstens ein Element ist, ausgewählt aus der aus den Gruppen IIA und IIIA, Gruppe VA,

Gruppe VIII, Ag, Au, Gruppen IIIB bis VIIB, der Lanthan-Reihe und der Actinium-Reihe bestehenden Gruppe,

$0,001 < b < 500$;

$0,001 < c < 500$;

$0 \leq d < 200$; und

x jene Anzahl von Sauerstoffatomen darstellt, die zur Befriedigung der Valenzerfordernisse der anderen Elementen nötig ist.

2. Verfahren nach Anspruch 1, worin Tetrahydrofuran und gamma-Butyrolacton gebildet werden.

3. Verfahren nach Anspruch 1, worin die Reaktionszeit weniger als 1 Minute beträgt.

4. Verfahren nach Anspruch 3, worin der Hydrierkatalysator mehr als 10 Gew.-% Aluminium enthält.

5. Verfahren nach Anspruch 4, worin der Hydrierkatalysator mehr als 15 Gew.-% Aluminium enthält.

6. Verfahren nach Anspruch 1, worin das Verhältnis von Wasserstoff zu Anhydrid-Einsatzmaterial von 10:1 bis 1000:1 beträgt.

7. Verfahren nach Anspruch 6, worin das Verhältnis von Wasserstoff zu Anhydrid-Einsatzmaterial von 50:1 bis 500:1 beträgt.

8. Verfahren nach Anspruch 1, worin die Hydrierung bei einem Druck von 1,0332 bis 103,32 kg/cm² (1 bis 100 Atmosphären) und bei einer Temperatur von 220° C bis 400° C ausgeführt wird.

9. Verfahren nach Anspruch 8, worin die Hydrierung bei einem Druck von 1,0332 bis 51,66 kg/cm² (1 bis 50 Atmosphären) und bei einer Temperatur von 220° C bis 300° C ausgeführt wird.

10. Verfahren nach einem der Ansprüche 1 bis 9, worin der Katalysator die gemischten Oxide von Kupfer, Zink, Aluminium umfaßt und gegebenenfalls Chrom, Eisen, Nickel und Kobalt enthält.

11. Verfahren nach Anspruch 10, worin der Katalysator die gemischten Oxide von Kupfer, Zink und Aluminium in Abwesenheit von Chrom umfaßt.

12. Verfahren nach Anspruch 10, worin der Katalysator die gemischten Oxide von Kupfer, Zink und Aluminium in Abwesenheit von Eisen umfaßt.

13. Verfahren nach Anspruch 10, worin der Katalysator die gemischten Oxide von Kupfer, Zink und Aluminium in Abwesenheit von Nickel umfaßt.

14. Verfahren nach Anspruch 10, worin der Katalysator die gemischten Oxide von Kupfer, Zink und Aluminium in Abwesenheit von Kobalt umfaßt.

Revendications

1. Procédé continu à une seule étape pour la préparation de tétrahydrofuranne ou de tétrahydrofuranne et de gamma-butyrolactone, comprenant l'hydrogénation catalytique d'un mélange sous forme de vapeur d'au moins un composant anhydride maléique ou anhydride succinique dans un gaz contenant de l'hydrogène au contact d'un catalyseur unique d'hydrogénation de formule :



dans laquelle M est au moins un élément choisi dans les Groupes IIA et IIIA, le Groupe VA, le Groupe VIII, Ag, Au, les groupes IIIB à VIIB, la série du lanthane et la série de l'actinium,

$0,001 < b < 500$;

$0,001 < c < 500$;

$0 \leq d < 200$; et

x est le nombre d'atomes d'oxygène nécessaire pour satisfaire aux conditions de valence des autres

éléments.

2. Procédé suivant la revendication 1, dans lequel du tétrahydrofuranne et de la gamma-butyrolactone sont produits.
- 5 3. Procédé suivant la revendication 1, dans lequel la durée de réaction est inférieure à 1 minute.
4. Procédé suivant la revendication 3, dans lequel le catalyseur d'hydrogénation contient plus de 10 % en poids d'aluminium.
- 10 5. Procédé suivant la revendication 4, dans lequel le catalyseur d'hydrogénation contient plus de 15 % en poids d'aluminium.
6. Procédé suivant la revendication 1, dans lequel le rapport de l'hydrogène à la charge d'anhydride a une valeur de 10:1 à 1000:1.
- 15 7. Procédé suivant la revendication 6, dans lequel le rapport de l'hydrogène à la charge d'anhydride a une valeur de 50:1 à 500:1.
- 20 8. Procédé suivant la revendication 1, dans lequel l'hydrogénation est conduite à une pression de 1,0332 à 103,32 kg/cm² (1 à 100 atmosphères) et à une température de 220 à 400 °C.
9. Procédé suivant la revendication 8, dans lequel l'hydrogénation est conduite à une pression de 1,0332 à 51,66 kg/cm² (1 à 50 atmosphères) et à une température de 220 à 300 °C.
- 25 10. Procédé suivant l'une quelconque des revendications 1 à 9, dans lequel le catalyseur comprend les oxydes mixtes de cuivre, zinc, aluminium et contient facultativement du chrome, du fer, du nickel et du cobalt.
- 30 11. Procédé suivant la revendication 10, dans lequel le catalyseur comprend les oxydes mixtes de cuivre, de zinc et d'aluminium en l'absence de chrome.
12. Procédé suivant la revendication 10, dans lequel le catalyseur comprend les oxydes mixtes de cuivre, zinc et aluminium en l'absence de fer.
- 35 13. Procédé suivant la revendication 10, dans lequel le catalyseur comprend les oxydes mixtes de cuivre, zinc et aluminium en l'absence de nickel.
- 40 14. Procédé suivant la revendication 10, dans lequel le catalyseur comprend les oxydes mixtes de cuivre, zinc et aluminium en l'absence de cobalt.